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Dated 8 July 2004

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1.	Your reference	P33300-/MGO/CWA		
2.	Patent application number (The Patent Office will fill in this part)	0 4 JUR 2003	0312781	.8
3.	Full name, address and postcode of the or of each applicant (underline all surnames)	Ythan Environmenta Unit 1, Castle Street Castlepark Industrial Ellon	•	
	08645020001	AB41 9RF		•
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	If the applicant is a corporate body, give the country/state of its incorporation	United Kingdom	•	
4.	Title of the invention	"Method"		
<u>-</u> 5.	Name of your agent (if you have one)	Murgitroyd & Compa	any	
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a) any applicant named in part 3 is not an inventor, orb) there is an inventor who is not named as an

c) any named applicant is a corporate body.

2 This invention relates to a method of insulating 3 submerged conduits, particularly but not exclusively those adapted to transfer fluids from subsea 5 hydrocarbon reservoirs to a service platform. 6 7 A plurality of conduits or pipes of relatively small 8 diameter typically extend from a seabed structure to 9 a service platform and are enclosed within an outer 10 'carrier' pipe. Such an arrangement is known as a 11 'pipeline bundle', and is adapted to convey produced 12 fluids from the well. 13 14 When fluids are extracted from subsea reservoirs, 15 their temperature is normally higher than that of 16 the surrounding water. As the fluids cool in the 17 pipes to the temperature of the water, certain 18 compounds come out of solution, and this causes 19 problems with precipitates such as waxes or gas 20 hydrates that build up within the pipelines and can 21

METHOD

2

reduce or prevent the flow of hydrocarbons. 1 Moreover, the viscosity of the produced fluids 2 increases as their temperature decreases, which also 3 reduces the rate of flow through the pipeline. 4 5 It is known to insulate pipeline bundles in several 6 ways to offset these problems - for instance pipes 7 are often insulated using solid synthetic foam 8 preformed insulating coatings. Alternatively the 9 pipe-in-pipe annular spaces are evacuated, or are 10 filled with silica-based materials or hollow spheres 11 of plastic material in a synthetic resin matrix. 12 13 These and similar techniques have serious 14 disadvantages in the way of investment cost, 1.5 difficulty of handling, and the requirement for 16 specialist equipment to manufacture the materials, 17 and as a consequence the materials needed for the 18 techniques are not routinely made up at the point of 19 manufacture of the pipeline. Also some of the 20 materials needed for the insulation are limited with 21 respect to the depth of water in which they can be 22 applied. For example, at depths beyond around 1500 23 metres the hydrostatic pressure of the water column 24 will collapse foam and its insulating qualities will 25 be lost. 26 27 A further attempt to solve this problem is disclosed 28 in European Patent Publication Nº 0,336,493. 29 this application, a liquid hydrocarbon gel is 30 provided in the outer pipe to insulate the smaller 31 diameter pipes running therethrough. However, the 32

use of a fluid gel requires the provision of a 1. pressure balancing system which is prone to failure. 2 3 Acording to the present invention, there is provided 4 a method of insulating a conduit, the method 5 comprising: 6 7 injecting a substance into a first conduit, the 8 first conduit enclosing at least one second 9 conduit; 10 11 allowing said substance to form a gel which has 12 a dynamic viscosity of more than 2000Pa.S. 13 14 Preferably, the conduits are tubulars, such as 15 oilfield tubulars. 16 17 Preferably, the substance is injected into an 18 annular space between the first and second conduits. 19 20 Preferably, the gel can retain its integrity 21 22 unsupported. 23 In this context, 'retain its integrity unsupported' 24 means a gel that can, for example, be sliced into 25 pieces and can maintain its form when dropped from a 26 height, but cannot be poured or pumped. 27 28 Preferably, the substance is a pourable fluid prior 29 to gellation. 30

Dynamic viscosities of gelled materials discussed in this patent are considerably in excess of 1000 Pa.S, preferably 2000 Pa.S - 100,000 Pa.S. Preferably, the substance comprises a fluid which has a comparatively high specific heat capacity and a second fluid which has a comparatively low thermal conductivity. More preferably, the first fluid is water and the second fluid is a a hydrophobic fluid such as a hydrocarbon-containing fluid or a vegetable oil. The relative proportons of the first and second fluids can be adjusted depending on the nature of the hydrocarbons being recovered, the specific pipeline arangement and the subsea environnement. Preferably, the substance further comprises a first and second polymeric compound. The first polymeric material may have a general formula

wherein A and B are the same or different wherein at least one comprises a relatively polar atom or group and R^1 and R^2 independently comprise relatively nonpolar atoms or groups.

Preferably, R1 and R2 are hydrogen atoms although they may be other relatively non-polar atoms or groups, for example, alkyl groups. Preferably, A and B are independently selected from optionally-substituted alkyl, cycloalkyl, cycloalkenyl, cycloalkynyl, aromatic and heteroaromatic groups. More preferably, A represents a phenyl group substituted, preferably at the 4-position relative to the group C-C, by a formyl group or a group of general formula: OR3 wherein x is an integer from 1 to 6 and each R^3 is independently an alkyl or phenyl group or together form an alkalene group. More preferably, group B represents a group of general formula:

X-

wherein R4 represents a hydrogen atom or an alkyl or 1 aralkyl group, R5 represents a hydrogen atom or an 2 alkyl group and X represents a strongly acidic ion. 3 4 Other options for the groups A, B and R1 - R5 are 5 disclosed in British Patent Publication GB 6 2.317,895A the disclosure of which is incorporated 7 herein by reference. 8 9 Preferably, the second polymeric substance includes 10 one or more functional groups capable of reacting 11 with said first polymeric compound. 12 13 More preferably, the second polymeric compound 14 includes a functional group selected from an 15 alcohol, carboxylic acid, carboxylic acid 16 derivative, for example an ester, and an amine 17 18 group. 19 Even more preferably, the second polymeric substance 20 is selected from optionally substituted 21 polyvinylalcohol, polyvinylacetate, polyalkalene 22 glycols and collagen (and any component thereof). 23 24 Yet more preferably the second polymeric material is 25 polyvinyl alcohol. Other possible second polymeric 26 materials are disclosed in the aforementioned 27 British Patent Publication 2,317,895A. 28 29 The substance may further comprise acid, such as 30 paratoluene sulphuric acid, to catalyse the reaction . 31

between the first and the second polymeric 1 compounds. 2 3 In alternative embodiments, the substance may 4 comprise a third polymeric material and a ferric 5 salt in addition to a hydrocarbon. Such alternative 6 embodiments preferably do not comprise the first and 7 second polymeric compounds nor water. Preferably 8 therefore, the alternative embodiments are effected 9 in a hydrocarbon phase. 10 11 Preferably, the third polymeric material is a 12 phosphate, more preferably an orthophosphate, even 13 more preferably an orthophosphate ester. 14 Preferably, the orthophosphate esters have the 15 structure of formula: 16 17 о || |---ок 18 19 wherein R is a straight or branched chain alkyl or 20 alkaryl group having about 6 to about 18 carbon 21 atoms and R' is hydrogen or an aryl, alkaryl or 22 alkyl group having about up to 18 carbon atoms. 23 24 Preferably, about 0.3% to 1.5 wt% by weight, based 25 on the hydrocarbon/water liquid, of the phosphate is 26 27 added. 28 Preferably, the ferric salt and third polymeric 29 material are added in an equimolar ratio. 30 preferably, the alternate embodiment forms a gel as 31

described in US Patent 5,417,287, the disclosure of 1 which is incorporated herein by reference. 2 3 4 Preferably, materials which undergo a change in 5 phase (such as going from liquid to solid) on cooling are selected, as these release heat thereby 6 7 extending the time it takes for the tubular contents to cool down. 8 9 Optionally, cenospheres may be added to the 10 substance in order to reduce thermal conductivity 11 12 and improve mechanical strength. 13 Optionally, antibacterial agents and/or corrosion 14 15 inhibitors can be added to the substance. 16 17 According to a second aspect of the present invention, there is provided a method of insulating 18 19 a submerged conduit, the method comprising the steps of: 20 applying at least one substance to the conduit 21 before it is submerged; then, 22 submerging the conduit under water; and 23 24 allowing the substance to form a gel. 25 26 Preferably the method employs the methods set out 27 above. 28 Preferably, the tubular comprises further tubulars 29 30 enclosed therein.

Preferably, the substance is applied to an annulus 1 between the tubular and the said further tubulars 2 enclosed therein. 3 4 Embodiments of the present invention will now be 5 described by way of example only. 6 7 Example 1 8 9 To test the effectiveness of such a gelled fluid 10 insulating system as an insulator for a pipeline 11 bundle the following experiment was carried out. 45g 12 of oil (for example sunflower or vegetable oil) were 13 placed in a container to which 35g of cenospheres 14 were added and the mixture was stirred for five 15 minutes until the cenospheres were fully dispersed. 16 17 Cenospheres are small glass hollow spheres of 18 between 20 - 150 microns such as can be extracted 19 from volcanic ash or the ash from coal-fired power 20 stations. The addition of cenospheres reduces 21 thermal conductivity and improves mechanical 22 strength of the resulting gel. However they are not 23 essential to the invention. 24 25 In a separate beaker a mixture of 18g of water and 26 2g of polyvinylalcohol (PVA) was made up and the 27 mixture of sunflower oil and cenospheres was poured 28 into this and mixed together to form an emulsion 29 mixture of oil, water, PVA and cenospheres. 30

British Patent publication GB 2,317,895A discloses a 1 substance and a method of forming a gel, the 2 disclosure of which is incorporated herein by 3 .4 reference. 5 An aqueous solution of 4-(4-formylphenylethenyl)-1-6 methylpyridinium methosulphonate (SbQ) was added to 7 the mixture as a cross-linking agent. The resulting 8 mixture was then stirred and the contents of the 9 beaker were decanted into a 100ml measuring 10 cylinder. An acid was then added to catalyse the 11 change of phase of the mixture from liquid to gel. 12 An inorganic or organic acid may be used, examples 13 being hydrochloric acid, sulphuric acid, acetic 14 The greater the quantity of acid, and formic acid. 15 acid which is used, the quicker the rate of 16 formation of the gel. Thus the rate of formation of 17 the gel can be controlled by varying the amount of 18 The mixture was allowed to stand for a acid used. 19 period of twelve hours after which time a reaction 20 had occurred and a gel had formed. 21 22 An aldol condensation reaction between polymer 23 chains is effected to form the gel, that is a 24 reaction between the polyvinylalcohol and the SbQ 25 according to the reaction scheme below: 26 27 28 29 30 31

1	
2	
3	он он он он он он
4	+
5	, С—H
6	, , H
7	
8	
9	V [±] -CH ₃
10	CH ₅ —N
11	СНО
12	CHO
13	N-CH ₃
14	H+
15	
16	он он о он он он
17	Ç n
18	
19	
20	N±_CH ₃
21	CH5—N
22	СНО
23	СНО
24	V [±] −CH ₃
25	

A determination of this material's thermal conductivity was carried out using a Huskaflux non-steady-state probe. The density was measured and the specific heat capacity was calculated from existing known values for each constituent in order to

determine the thermal diffusivity of the gelled 1 system. 2 3 Table 1 below details the thermal performance of 4 5 example 1. 6 Example 2 7 8 A second gelled fluid insulating system containing 9 76.5g of water, 8.5g of polyvinyl alcohol, 10g of 10 sunflower oil and 5g of cenospheres was similarly 11 made up, following the method of example 1. 12 13 0.5g of SbQ and 1g of acid (HCl 10%) was then added. 14 15 After a period of time, typically between one and 16 twenty four hours, the mixture sets as a solid 17 jelly-like material by undergoing the equivalent 18 aldol condensation reaction detailed above. 19 20 Some properties of this gel are set out in table 1, 21 below. 22 23 Example 3 24 25 A third all oil system using different chemistry was 26 made up according to a method described in US patent 27 5,417,287 the disclosure of which is incorporated 28 herein by reference. 29 30 16g of cenospheres were stirred into a container 31 holding 84g of kerosene. To this mixture 1g 32

Clearwater HGA 70 (an orthophosphate ester) was 1 added (although between 0.3 and 1.5% by weight is 2 suitable). The mixture was gelled by the addition of 3 1g of Clearwater HGA 65 (a ferric salt). 4 Alternatively ferric sulphate may be added at 5 between 0.25 to 2.0 moles per mole of phosphate 6 ester. The fluid was left to gel for a period of 24 7 hours. In practice however a gel formed typically 8 between 2-5 minutes from adding the ferric source. 9 10 Some of the properties of this gel are set out in 11 table 1 below which also shows a range of gelled 12 fluid insulating systems with different mixes of 13 ' oil, water and cenospheres. 14 15 Example 4 16 17 A fourth gelled fluid insulating system containing 18 10g of water, 1g of polyvinyl alcohol, 45g of 19 sunflower oil and 45g of cenospheres was similarly 20 made up, following the method of example 1. 21 22 0.05g of SbQ and 1g of acid (HCl 10%) was then 23 added. 24 25 After a period of time, typically between one and 26 twenty four hours, the mixture sets as a solid 27 jelly-like material by undergoing the equivalent 28 aldol condensation reaction detailed above. 29 30 Some properties of this gel are also set out in 31 table 1, below.

1

2 In general the relative proportions of components in

3 the gelled fluid insulating medium were determined

4 using considerations of cost, ease of shipping to

5 manufacturing location and desired performance

6 characteristics.

7 8

Of particular interest is a measure of the rate of

c 9 cool down known as diffusivity, this is described

10 as:

11

Diffusivity = Conductivity (W/mK) / [Specific heat

13 capacity(J/kg/K) x Density kg/m3]

14

15 The diffusivity measurements are given in table 1

16 below.

Gel	Ratio of Components				Conducti vity ^[3]	Specific Heat ^[2]	Density ⁽²⁾	Diffusivity
	Oil	Water	Other	Cenosp heres	W/mK	J/kgK	kg/m³	m²/s
1	45	18	2 PVA + 0.125 SbQ + 1 acid	35	0.22	1870	908	0.130 x 10 ⁻⁶
2	10	76.5	8.5 PVA + 0.5 SbQ + 1 acid	5	0.44	3790	982	0.118 x 10 ⁻⁶
3	84 [4]	0	1 C'HGA 70 (phosphate ester) 1 C'HGA 65	16	0.14	1740	863	0.093 x 10 ⁻⁶
			(ferric					
4	45	10	1 PVA + 0.05 SbQ + 1 acid		0.17	1480	901	0.127 X 10 ⁻⁶

Table 1 1 2 Notes: Samples based on sunflower oil. 3 [1] Estimated from available data for constituents. 4 Conductivity was measured using a non steady state probe 5 6 7 [4] Oil based gel using paraffinic oil. 8 9 Abbreviations 10 PVA - Polyvinylalcohol SbQ - 4-(4-formylphenylethenyl)-1-methylpyridinium methosulphonate 11 12 OPE - Orthophosphate ester C'HGA 70 - Clearwater HGA 70 (phosphate ester) 13 C'HGA 65 - Clearwater HGA 65 (ferric salt) 14 15 The gelled fluid insulating media thermal 16 conductivities and diffusivities (a measure of the 17 rate of cool down) are comparable to those of 18 existing syntactic materials, which can go down to 19 0.12W\mK and 0.12X10 $^{-6}$ m 2 \s respectively. 20 low conductivity is required to provide the steady 21 state thermal performance on the flowing system, low 22 diffusivity is also desirable to maintain long cool-23 down times. 24 25 In use, the pipeline bundles are made up on the 26 surface as is conventional in the art and an 27 oil/water/additive mixtures for example, those 28 detailed in examples 1-4 above, are then added to 29 the pipe-in-pipe annular space between the inner 30 pipes and the carrier pipe. The bundles are then 31 installed in the conventional manner. 32 33 The mixture has a sufficiently low viscosity to 34 enable it to be pumped into the pipe-in-pipe bundle 35 annular space where a reaction can take place which 36 results in the mixture forming into a gel as defined 37 in the Larousse Dictionary of Science and Technology 38

1995 page 470, that is a substance with properties 1 intermediate between the liquid and the solid 2 3 states. 4 The resulting gelled material is a jelly-like 5 substance and so can transmit the hydrostatic 6 pressure upon the external tubular or 'carrier' to 7 the inner tubulars. A further benefit of certain 8 embodiments of the present invention in using such 9 gelled fluid insulating media in pipe-in-pipe 10 systems is therefore that the external carrier pipe 11 does not need to be rated to hydrostatic pressure 12 experienced at depth since the gelled fluid 13 insulating media transfers the hydrostatic pressure 14 onto the inner tubulars. 15 16 A further consequence of certain embodiments of the 17 invention transmitting pressure is that they 18 maintain their integrity and insulating properties 19 unlike some prior art systems which can collapse and 20 lose their insulating properties at higher pressure. 21 Thus embodiments of the present invention do not 22 suffer the same depth limitations as syntactic foams 23 (although they will deform and recover at higher 24 stress). 25 26 The formation of a gel acts to prevent loss of heat 27 through convection. An advantage of certain 28 embodiments of the present invention is that the gel 29 possesses low conductivity, thereby providing 3.0 suitable insulating properties for deep water 31 applications. 32

1 A further advantage of certain embodiments of the 2 present invention is the high thermal mass and low 3 diffusivity of the gel which increases cool-down 4 5 times and gives operational flexibilty for long tiebacks and remote deep water production systems. 6 7 A further benefit of certain embodiments of the 8 present invention is that the thermal performance of 9 the gels, including conductivity and heat capacity, 10 can be varied and thus suitably tailored for 11 individual systems by varying the relative 12 components of oil, water and cenospheres. 13 different compositions of the gels are used 14 depending on the specific nature of the fluids being 15 transported, the pipeline arrangement, the subsea 16 17 environment and other factors. 18 For instance, example 2 has a high specific heat 19 capacity making it suitable for applications where a 20 long cool down performance is required. Example 4 21 by contrast has a much lower thermal conductivity 22 and so it would be particularly suited to ensure 23 high pipeline fluid arrival temperatures thereby 24 easing fluid processing. Example 3 offers a balance 25 between thermal conductivity and good cool down 26 27 performance although it has a less favourable 28 environmental profile. 29 30 A further benefit of certain embodiments of the present invention is the low toxicity and generally 31

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non-hazardous materials which are used which 1 facilitates handling, transportation and disposal. 2 3 Moreover, the cost of certain embodiments of the 4 present invention is less than previous syntactic 5 'wet' coatings or silica based pipe-in-pipe systems, 6 they can be made on site and do not require 7 expensive storage or mixing facilities and a 8 pressure-rated outer carrier pipe is not required. 9 10 The thermal properties can be improved further by 11 selecting materials that undergo a change in phase 12 (such as going from a liquid to a solid) on cooling. 13 This change in phase will result in the release of 14 heat thereby extending the time it takes for the 15 16 pipeline contents to cool down. 17 Other chemicals such as anti bacterial agents, for 18 example Dow™ Antimicrobial 7287, Avecia Proxel XL2 19 or Rhodia Tolcide PS50D, or corrosion inhibitors for 20 example imidazoline, amine salts or phosphate esters 21 can also be added to this gelled fluid insulating 22 23 medium. 24 25 Improvements and modifications may be made without 26 departing from the scope of the invention.